

Improved Design and Efficiency of the Extractive Distillation Process for Acetone-Methanol with Water

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Supporting information

Appendix S1 Sizing and economic cost calculation

The diameter of a distillation column is calculated using the *tray sizing* tool in Aspen Plus software.

The height of a distillation column is calculated from the equation:

$$H = \frac{N}{e_T} \times 0.6096 \quad N \text{ tray stage except condenser and reboiler, } e_T \text{ tray efficiency is taken as 100\% in}$$

this work.

The heat transfer areas of the condenser and reboiler are calculated using following equations:

$$A = \frac{Q}{u \times \Delta T} \quad u: \text{ overall heat transfer coefficient (kW} \cdot \text{K}^{-1} \cdot \text{m}^{-2}), u=0.852 \text{ for condenser, } 0.568 \text{ for}$$

reboiler.

The capital costs of a distillation column are estimated by the following equations:

$$\text{Shell cost} = 225228D^{1.066}H^{0.802}$$

$$\text{Tray cost} = 1423.7D^{1.55}H$$

$$\text{HeatExchanger cost} = 9367.8A^{0.65}$$

Table S1. Binary Interaction Parameters* for UNIQUAC Model of Acetone-Methanol-Water

Component i	Acetone	Acetone	Methanol
Component j	Methanol	Water	Water
A _{ij}	0	8.6051	-1.0662
A _{ji}	0	-4.8338	0.6437
B _{ij}	-225.153	-3122.58	432.8785
B _{ji}	52.7705	1612.196	-322.131

* K unit, $\tau_{ij} = \exp(A_{ij} + B_{ij}/T + C_{ij}\ln T + D_{ij}T + E_{ij}/T^2)$

Table S2. Sizing parameters for the optimal designed columns and cost data from closed loop simulation for the extractive distillation of acetone – methanol with water

column	Case 1		Case 2b		Case 3opt	
	C ₁	C ₂	C ₁	C ₂	C ₁	C ₂
<i>Diameter</i> / m	2.88	1.92	2.66	1.77	2.88	1.72
<i>Height</i> / m	33.53	14.63	33.53	14.63	33.53	14.63
<i>I_{CS}</i> / 10 ⁶ \$	1.164	0.389	1.069	0.356	1.164	0.346
<i>A_C</i> / m ²	601	284	518	244	679	229
<i>A_R</i> / m ²	551	371	469	319	412	309
<i>I_{HE}</i> / 10 ⁶ \$	1.166	0.807	1.055	0.731	1.118	0.709
<i>Cost_{cap}</i> / 10 ⁶ \$	2.576	1.252	2.341	1.137	2.528	1.102
<i>Cost_{ope}</i> / 10 ⁶ \$	1.290	0.869	1.097	0.746	0.967	0.722
<i>Cost_{CA}</i> / 10 ⁶ \$	2.148	1.287	1.877	1.125	1.809	1.089
<i>Q_{HA}</i> / MW	1.24		0.91		0.58	
<i>Cost_{HA}</i> / 10 ⁶ \$	0.035		0.028		0.021	
TAC / 10 ⁶ \$	3.469		3.030		2.918	
OF / kJ/kmol	36247.5		30916.2		28318.5	